

# Sustainable Approaches for Abnormal Situation Management

*Presented by*

**Dr. Kazi Monzure Khoda**

**Department of Chemical Engineering**

**Qatar University**

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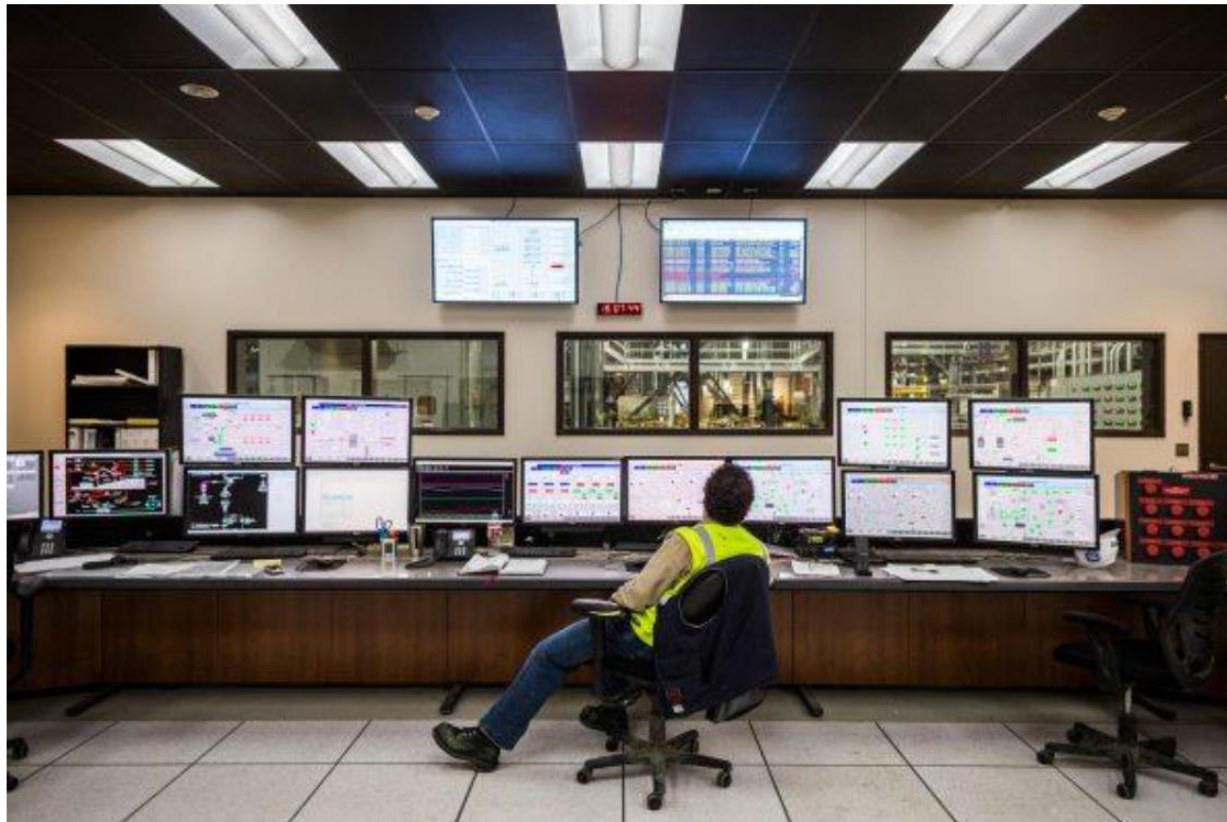


**Workshop on Energy & Water Security**  
**Doha, Qatar**



# Process Upsets – Abnormal Situations

Is this a Normal Situation?



# Process Upsets – Abnormal Situations

**Is this what we mean by Abnormal Situation?**



# Process Upsets – Abnormal Situations

Processes eventually deviate from normal operations; and *control system* are in place to *mitigate* such deviations.

When control system **CAN NOT** cope with disturbances, human intervention (DCS operators) is needed

**ABNORMAL  
SITUATIONS**



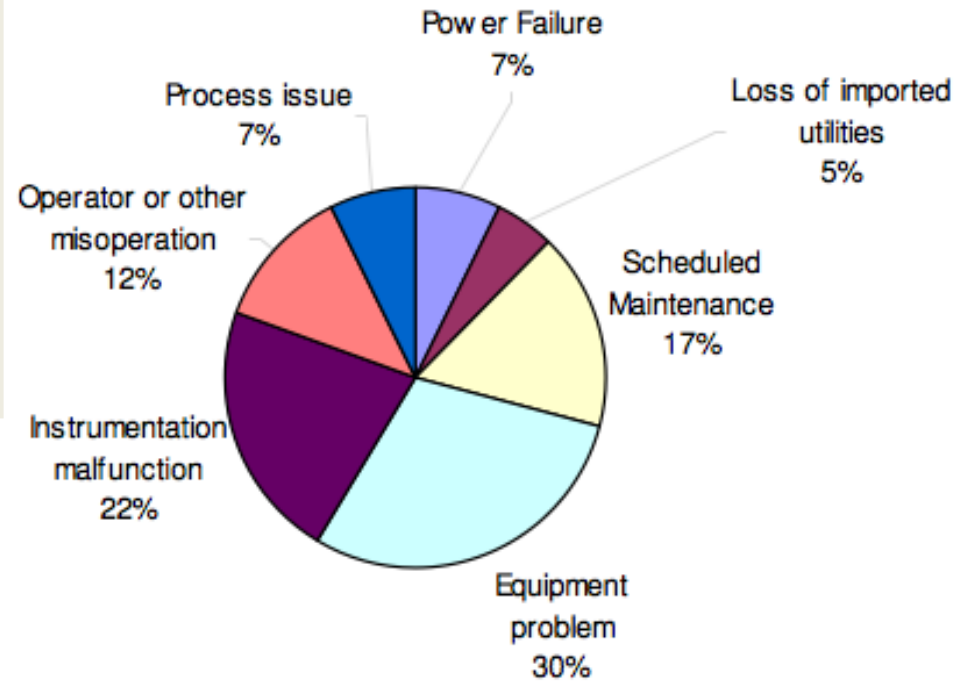
Cochran, E., Bullemer, P. (1996). "ASM: Not by New Technology Alone...", 1996 AIChE conference.

# Process Upsets – Abnormal Situations

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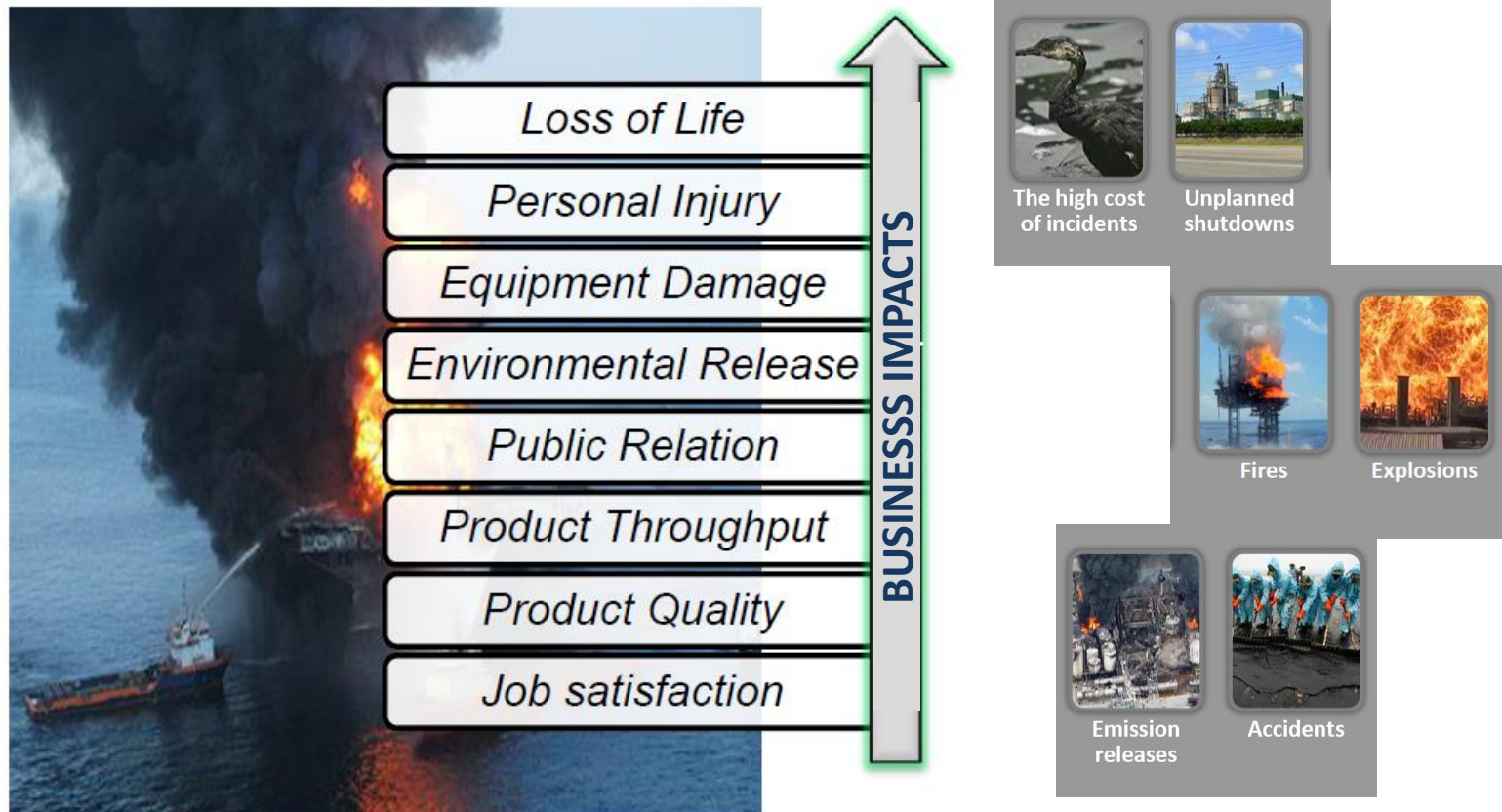
**ABNORMAL  
SITUATIONS**



Midstream Upset Flaring and Management Options, April 2010

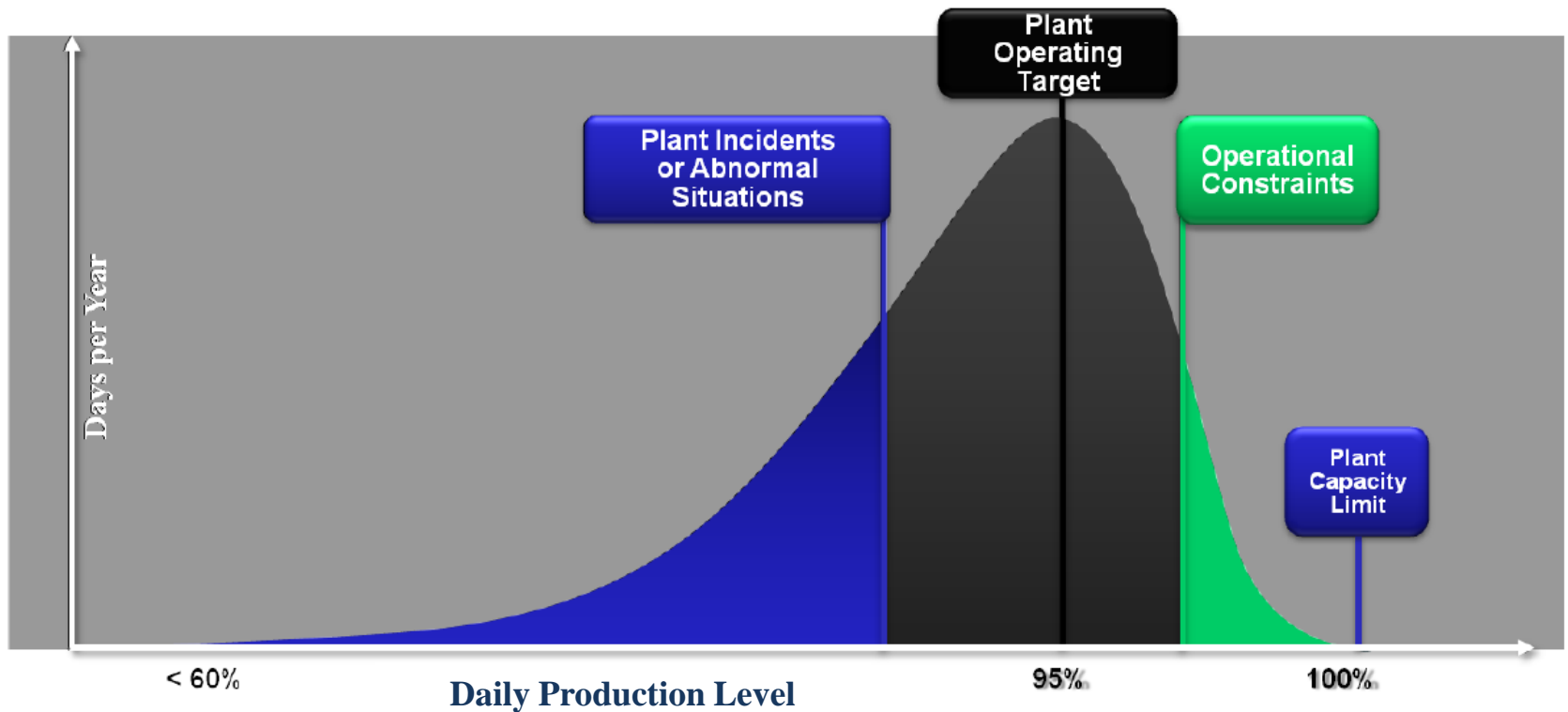
# Process Upsets – Abnormal Situations

## Abnormal Situations Impact Profitability



# Process Upsets – Abnormal Situations

## The Business Impact of Abnormal Situations

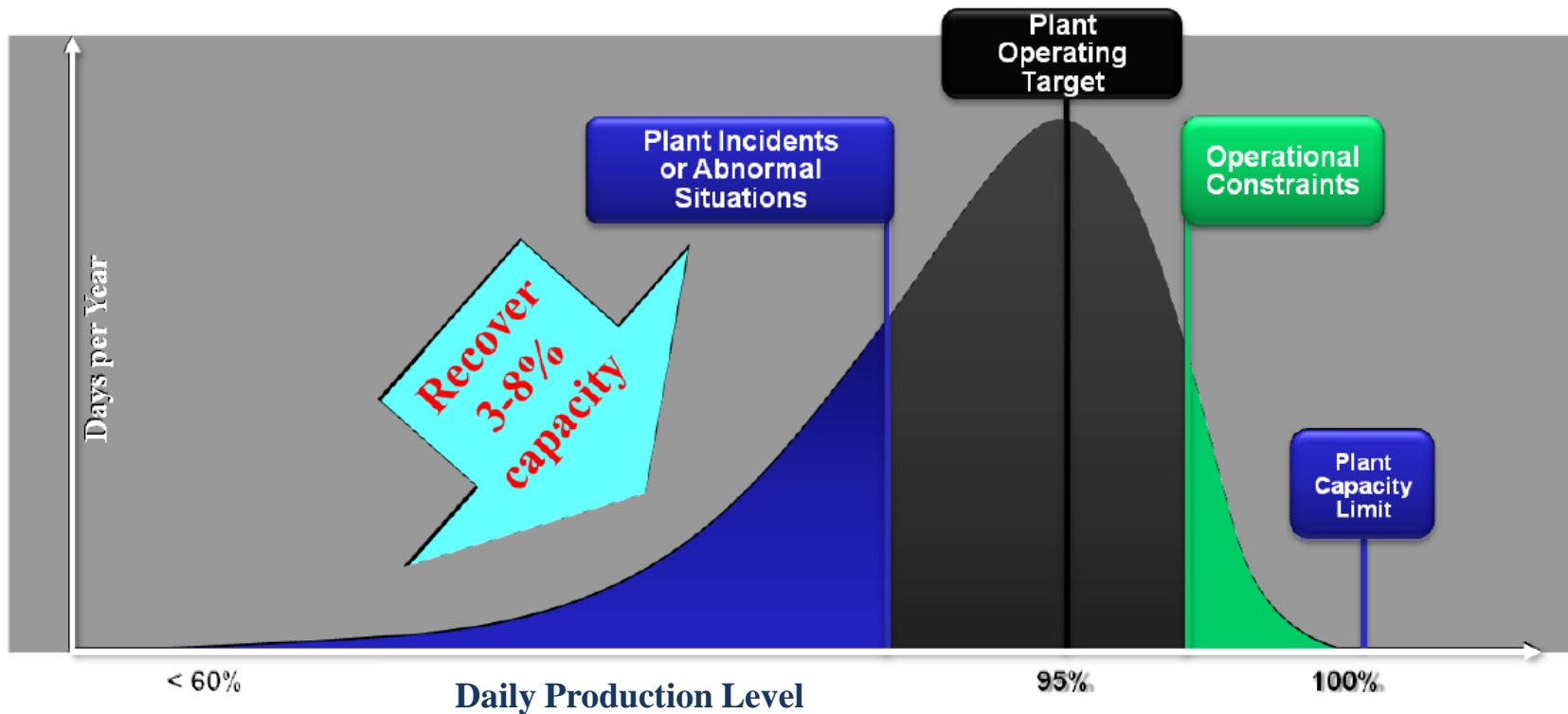


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*Unexpected Events can cost 3 – 8 % of Capacity*

# Process Upsets – Abnormal Situations

## The Effects of Managing Abnormal Situations



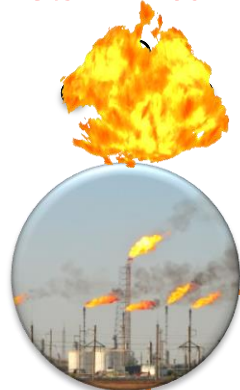
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*What is 1 hour, 1 day, 1% of capacity worth?*



# Flaring – Abnormal Situations

## Why Industries Flares?



### Process Safety

- Routinely small volumes of unrecoverable gases
- Managing excess gas production



### Process Upsets

- Equipment malfunction
- Off-spec production
- Depressurizing equipment
- Start-ups or Emergency shutdowns



### Disposal Associated Gases

- Oil production and gas processing facilities
- Insufficient infrastructure

# Flare Reduction – Why?

**Waste Valuable Resources**

**Negative Environmental Impacts**

**Unnecessary CO<sub>2</sub>/SO<sub>2</sub>/Nox emissions**

**Safety & Economics Impacts**

**Noise - Neighboring Communities**

**Visible to Surrounding Community**

**Visible black smoke and soot**

# Flare Reduction – Challenges?

- Reducing rates while production levels increase
- Cost effective alternatives
- Co-operation with neighboring/competing operators for joint facilities

*Global gas flaring has remained largely stable over the past fifteen years, in the range of 140 to 170 billion cubic meters (BCM)*



# Flare Reduction – How?

Legislation

Flare  
Recovery

Flare  
Utilization

Incentives

## Qatar's Proactive Legislative Acts

- '02 Establishing Supreme Council for the Environment
- '05 Kyoto Protocol & '07 AlShaheen CDM Project
- '09 World Bank Global Gas Flaring Reduction (GGFR)
- '12 COP Meeting



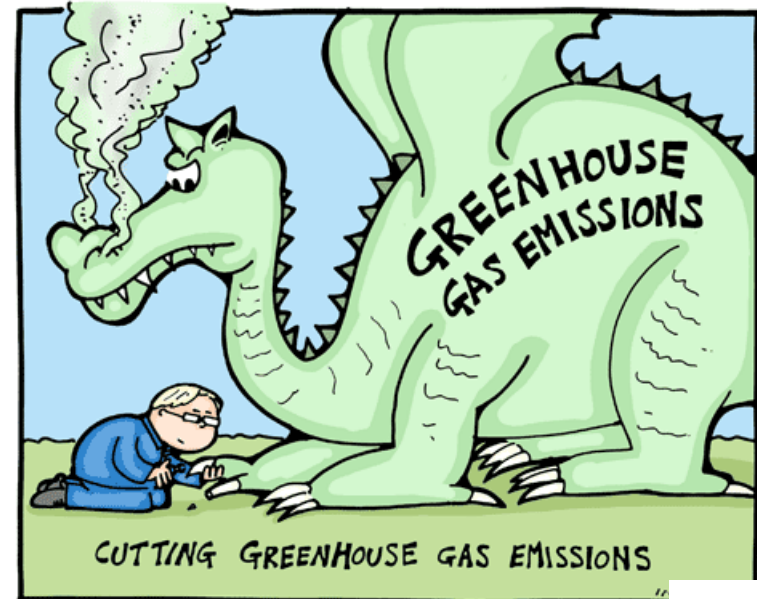
# Flare Reduction – How?

Legislation

Flare  
Recovery

Flare  
Utilization

Incentives



# Flare Management – Generic Approach

Identify key flaring sources due to upsets



Identify causes & consequences of process upsets

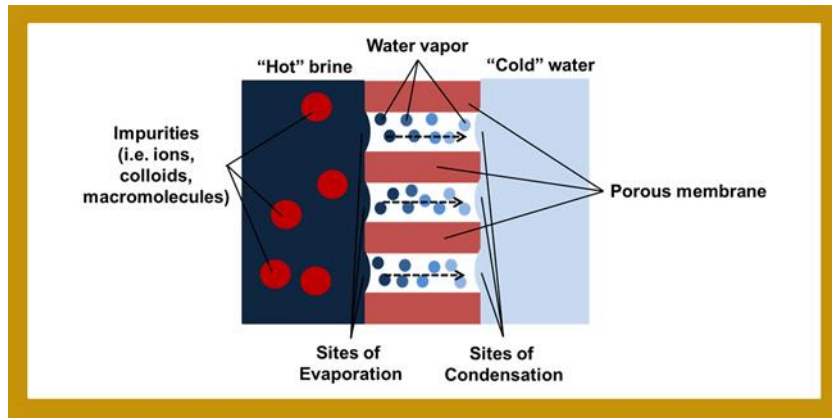
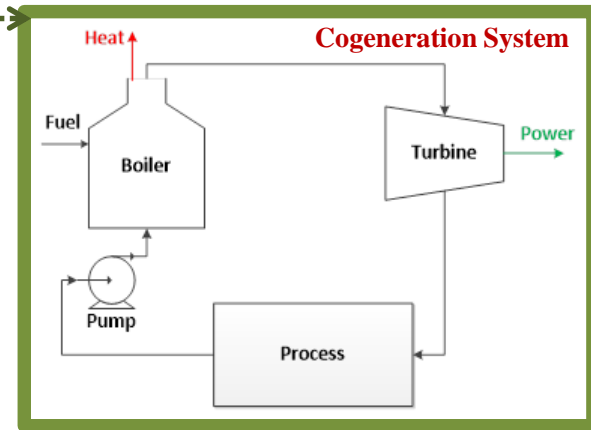
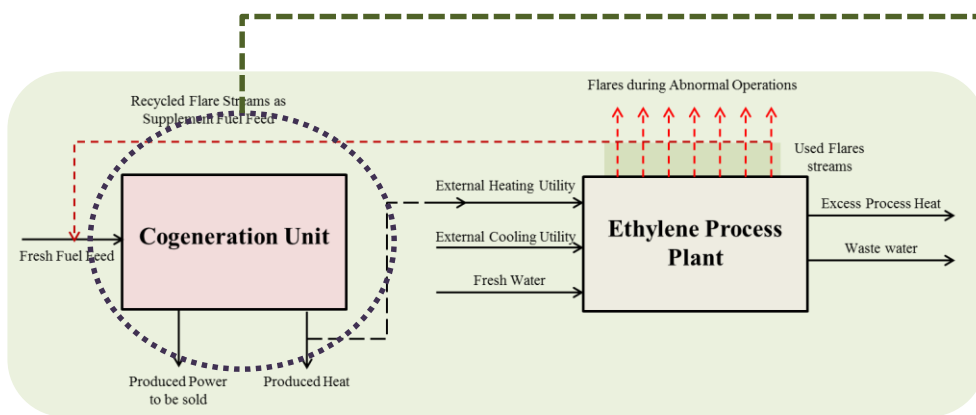


Apply recent process design/control and optimization methods

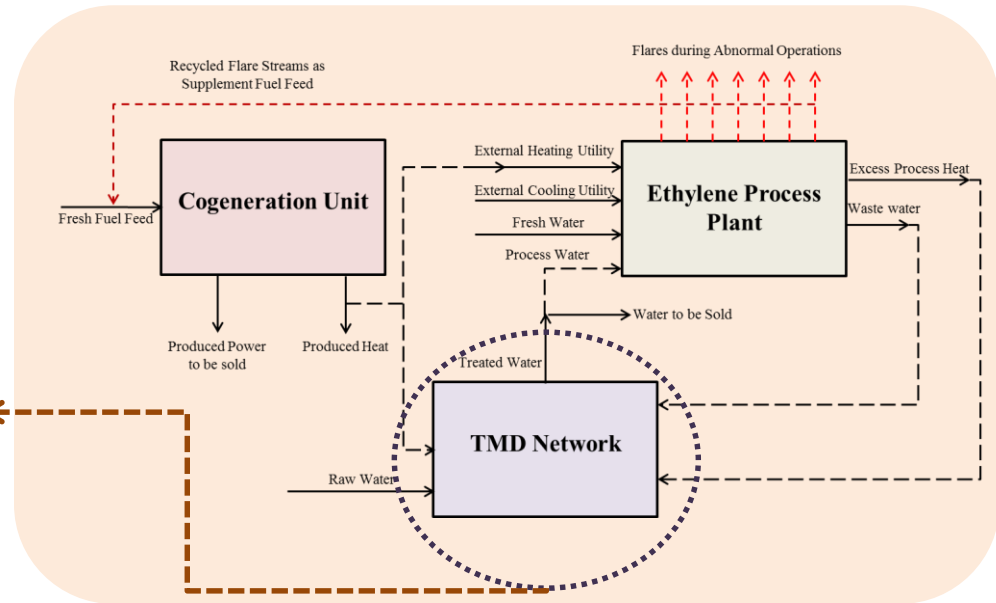


# Energy Integration Alternatives

## Proposed Alternatives for Managing Flare Streams

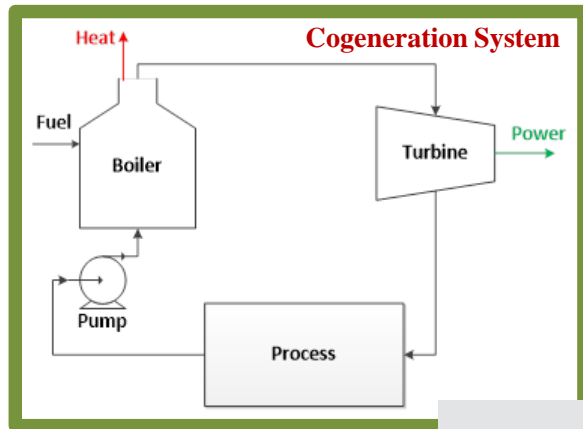


Thermal Membrane Distillation



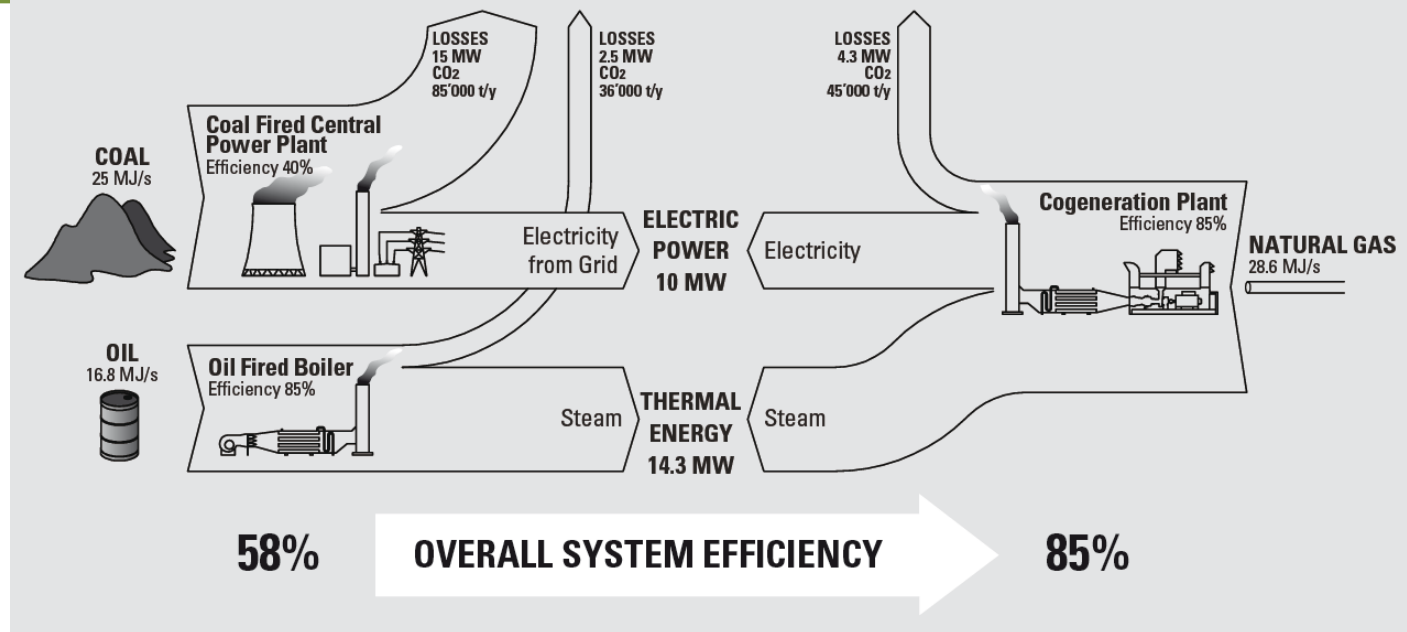
# COGEN Approach

## What is Cogeneration (COGEN)?



## Advantages of COGEN

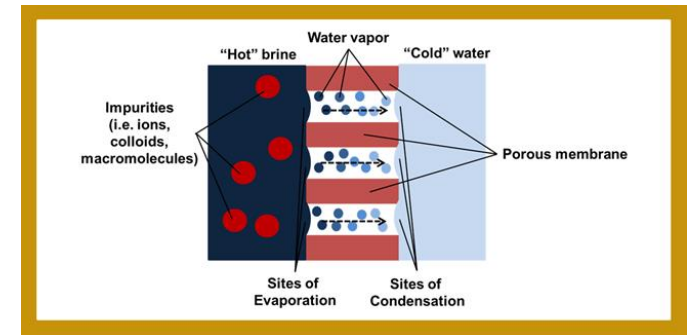
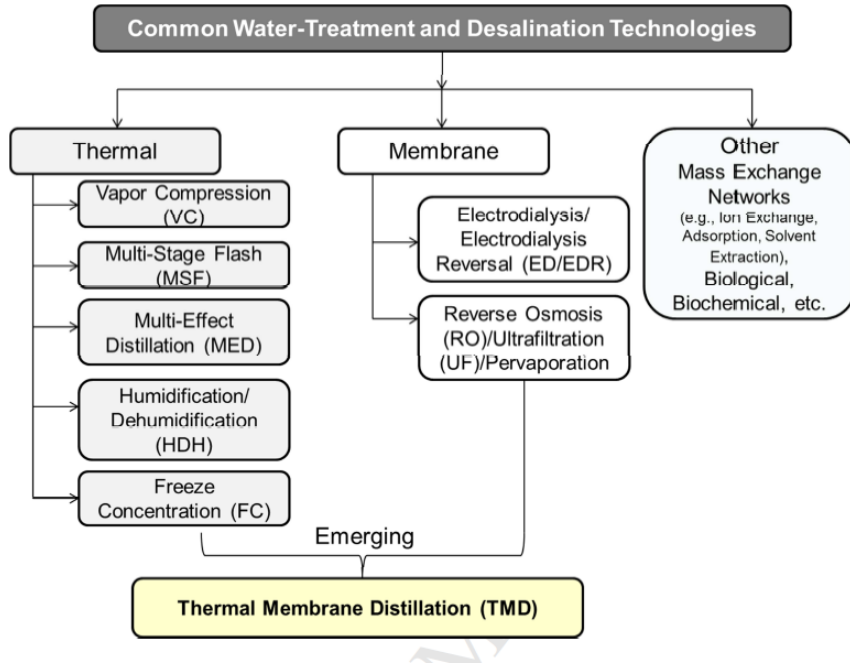
- Simultaneous generation of heat and power
- Reusing waste flare streams
- Carbon tax savings





# TMD Approach

## What is Thermal Membrane Distillation (TMD)?



Thermal Membrane Distillation

## Advantages of TMD

- Low level heating
- Moderate operating temperature and pressure
- Ability to treat highly concentrated feeds
- High –purity permeate products
- Compact size
- Modular nature

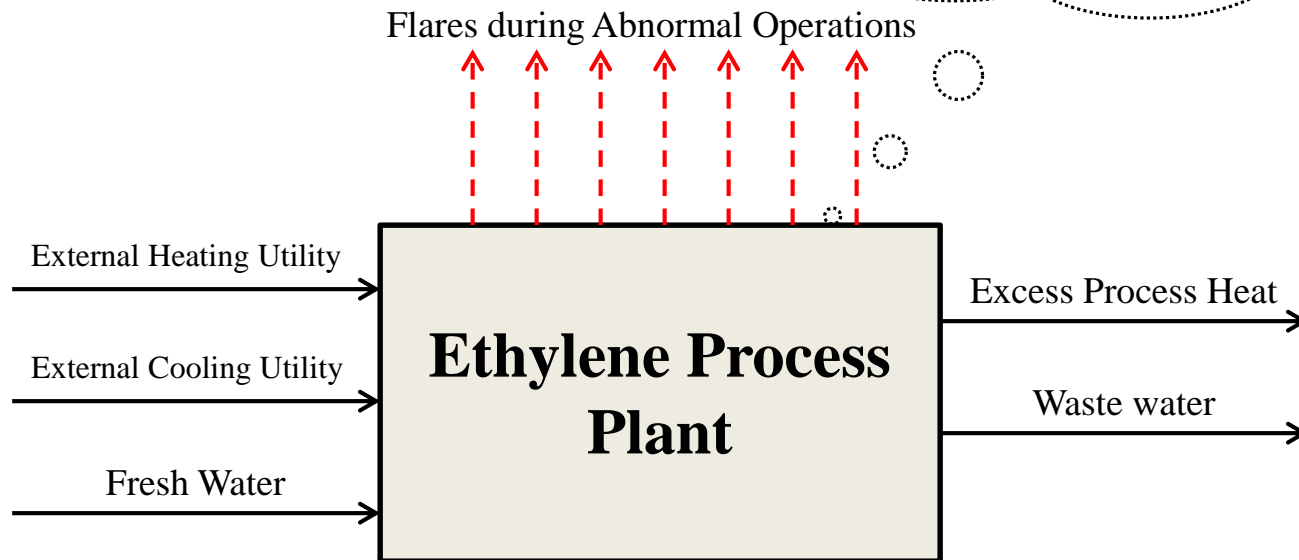
## Several Configurations of TMD

- Direct contact membrane distillation (DCMD)
- Vacuum membrane distillation
- Air gap membrane distillation (AGMD)
- Sweep gas membrane distillation (SGMD)

# Case Study

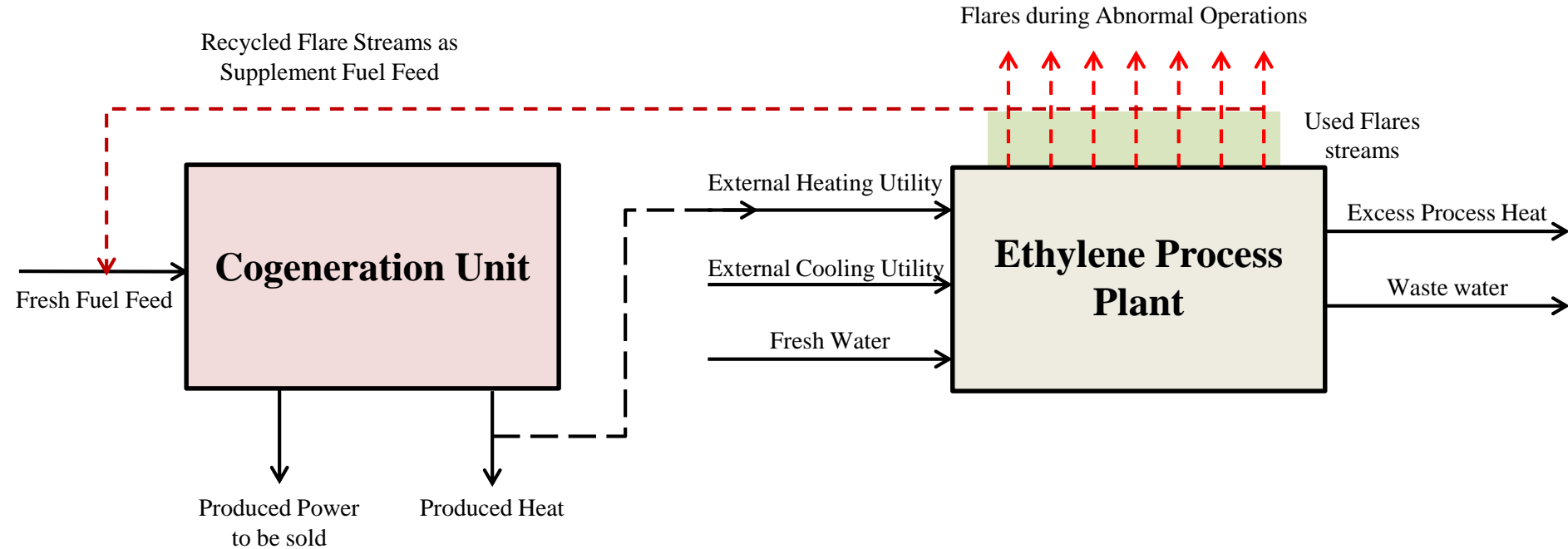
## Base Case Ethylene Process Plant

- Need extra cooling utility
- Need waste water treatment
- Unused Flare Streams

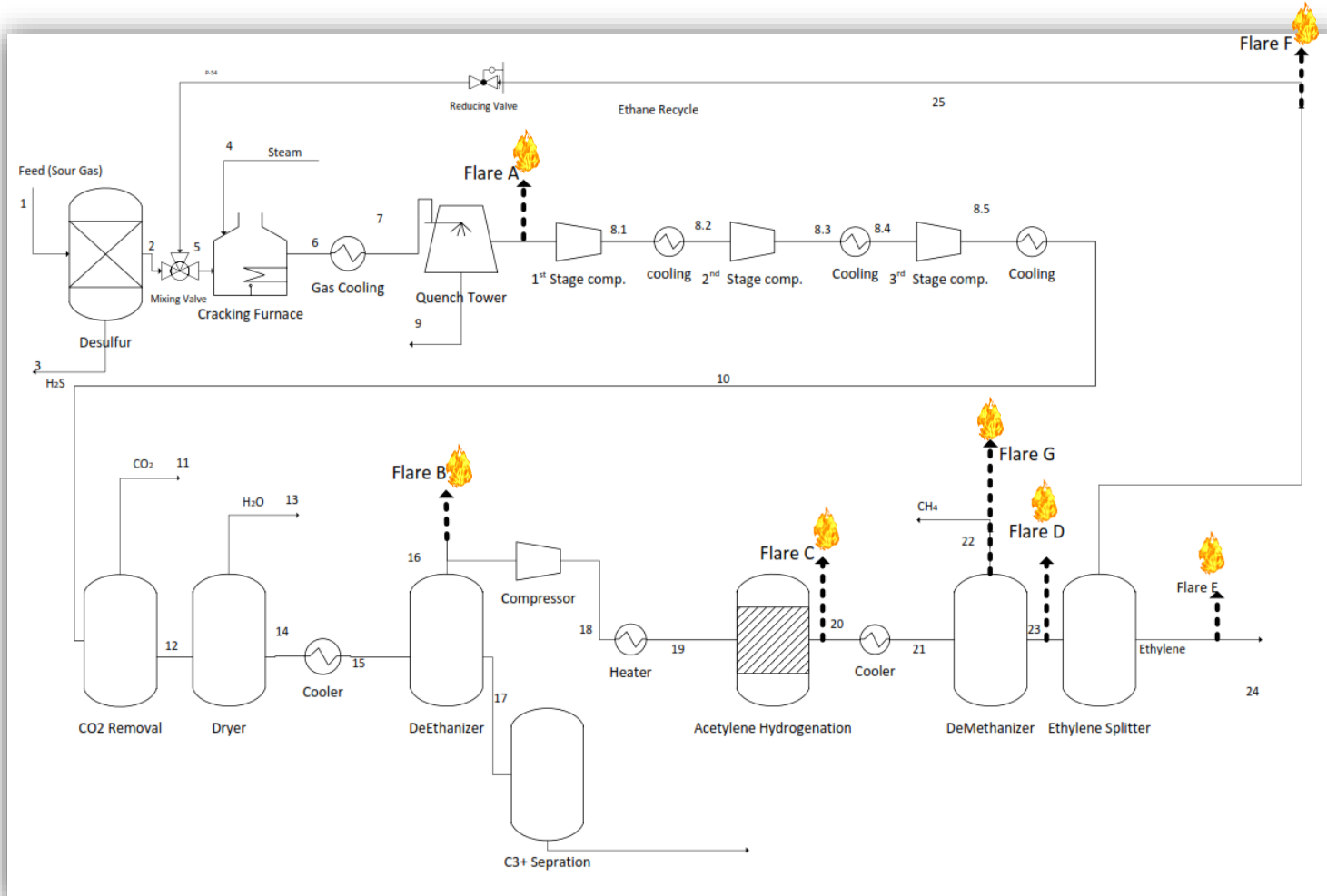


# COGEN Approach

## Flare Mitigation Approach using Cogeneration Unit



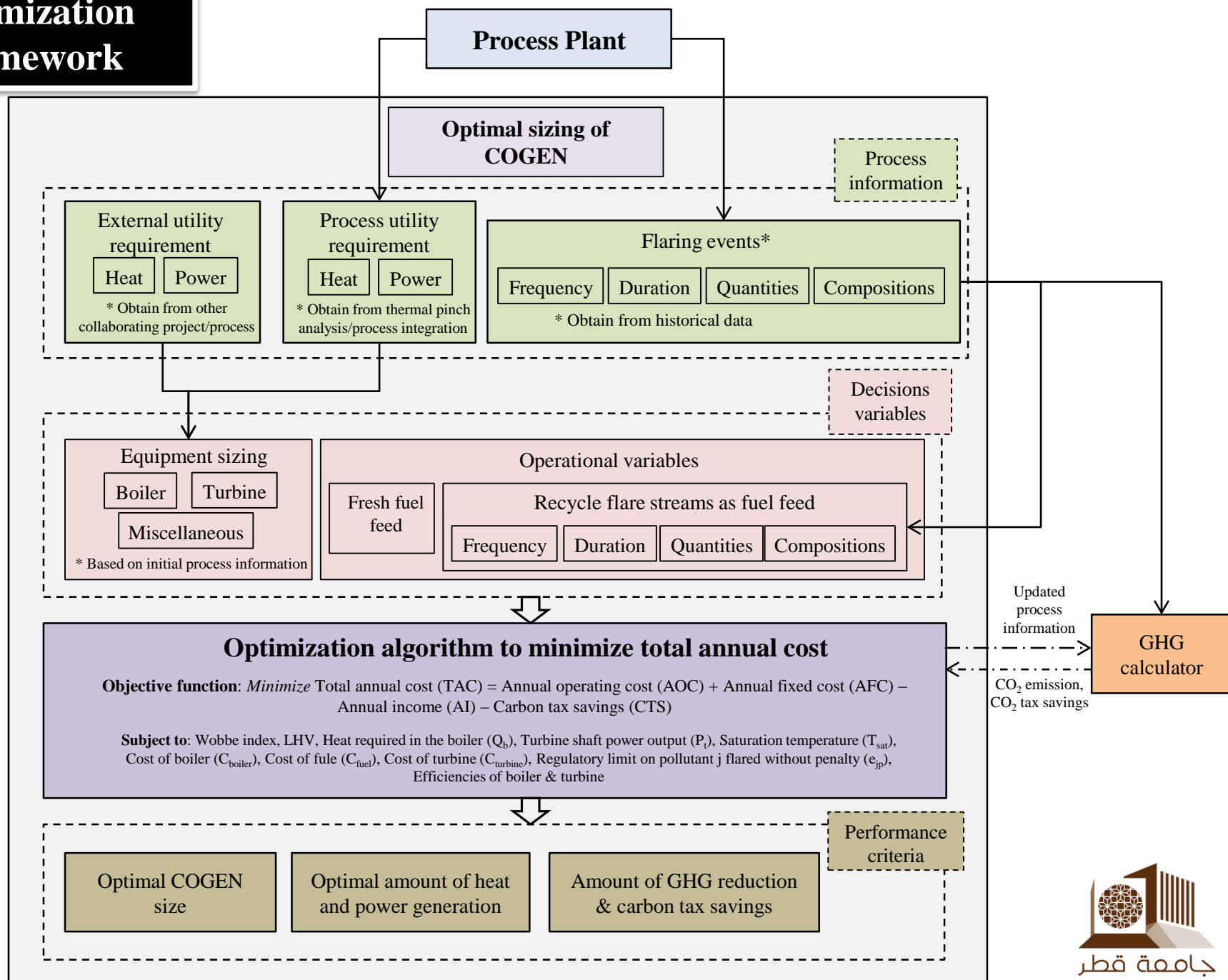
# Possible Flare Locations



Flare Name	Location
Flare A	Top of quench tower
Flare B	De-ethanizer overhead
Flare C	Acetylene hydrogenation outlet
Flare D	De-methanizer bottom product
Flare E	Off-spec Ethylene
Flare F	Ethylene splitter overhead/ Ethane Recycle
Flare G	De-methanizer overhead

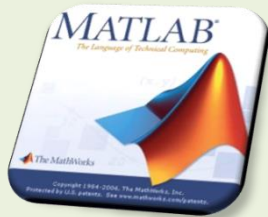
**Ethylene process base case with all possible flare locations**

# Optimization Framework



# Optimal Sizing of COGEN

- Platform: MATLAB
- Optimization toolbox: Genetic algorithm toolbox
- Advantage of optimization formulation: Generic and flexible

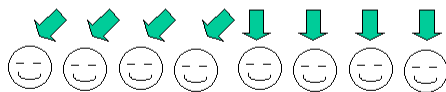


## Genetic Optimization



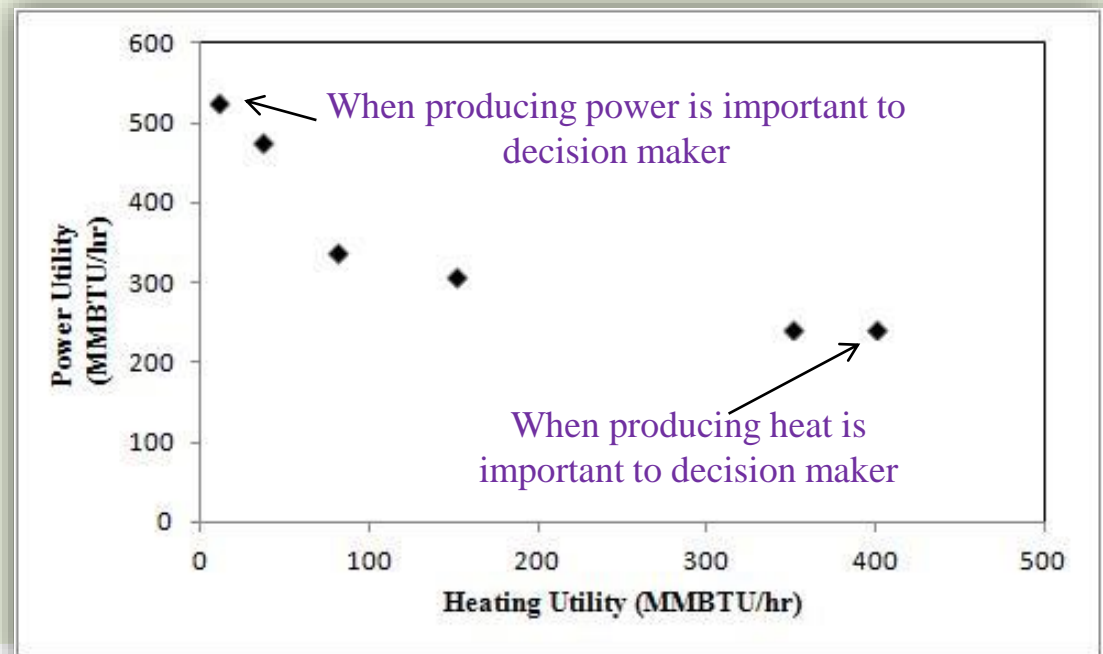
Out of the gene pool

Crossover



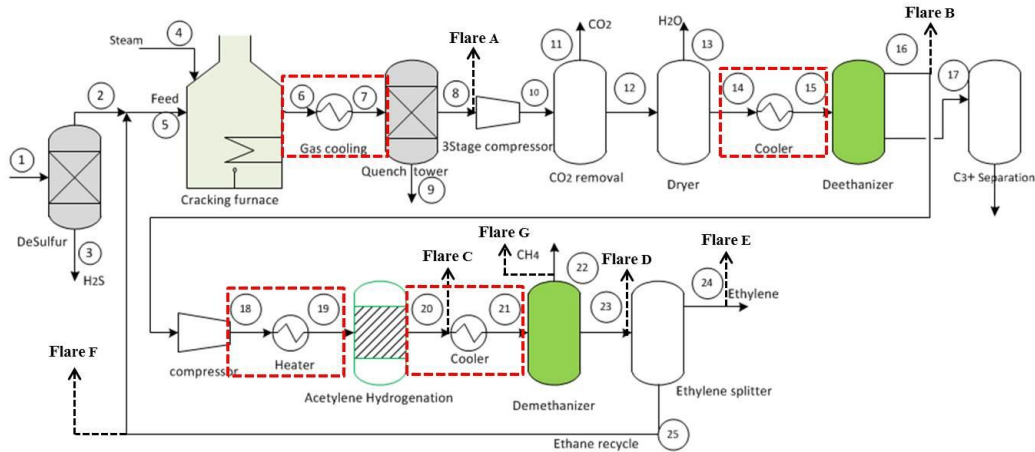
New generation of stronger candidates

## Pareto Fronts

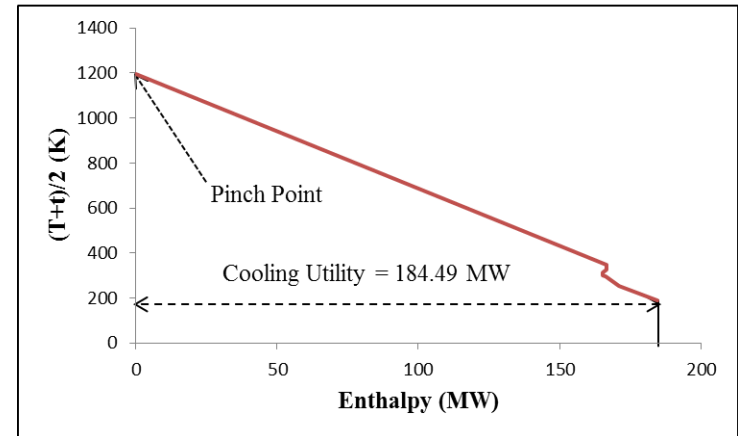


# TMD Approach

Why.....?



## Grand Composite Curve



Minimum cooling utility for our base case ethylene plant is :

**184.49 MW = 629.50 MMBtu/hr**

### Before Heat Integration

- Heating utility cost: \$1.53 MM/yr
- Cooling utility cost: \$24 MM/yr
- Total utility cost: \$25.53 MM/yr

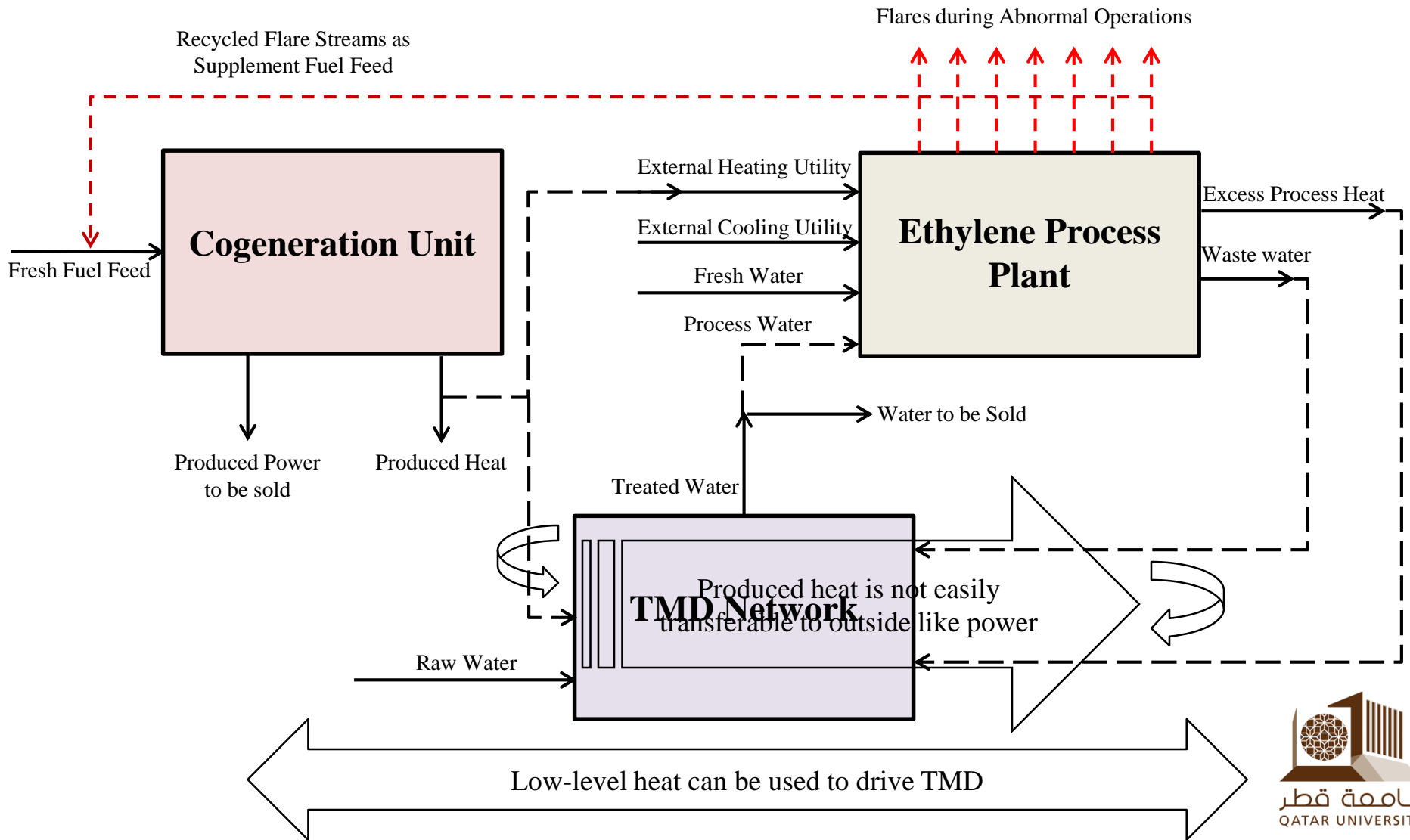
### After Heat Integration

- Heating utility cost: \$0 MM/yr
- Cooling utility cost: \$23 MM/yr
- Total utility cost: \$23 MM/yr

**Still the cooling utility cost is significant**

# TMD Approach

## Flare Mitigation Approach using COGEN Unit and Thermal Membrane Distillation Network



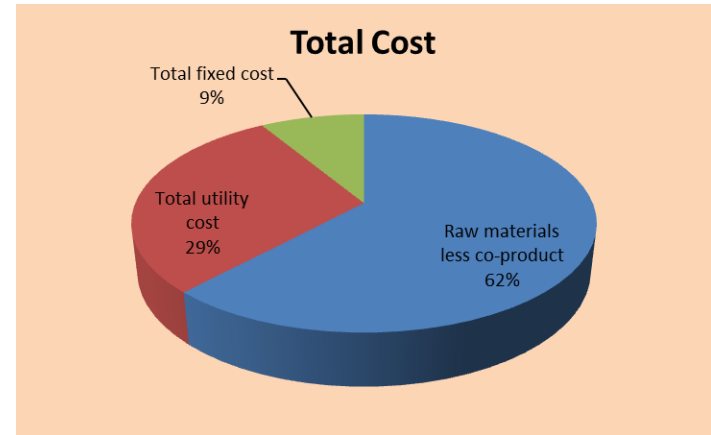


# Ethylene Production Cost

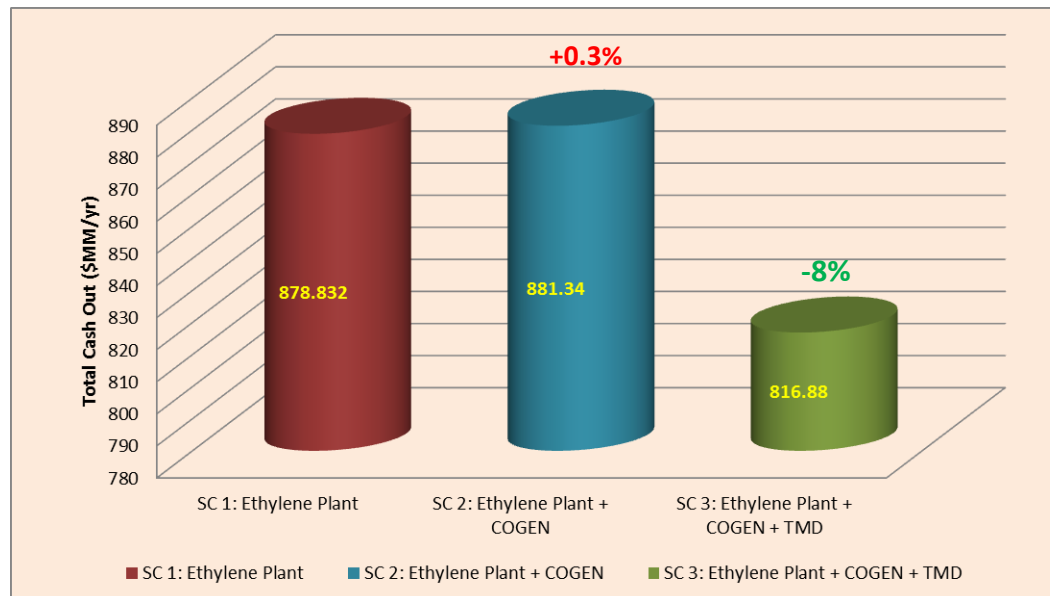
## Comparison between the Results for the Two Proposed Flare Mitigation Approaches for Existing Ethylene Plant

### Basis:

Ethylene production (ton/yr)	900000
Crude oil price (\$/bbl)	100
NG price (\$/MMBtu)	4
COGEN heating utility (MMBtu/hr)	400
COGEN power utility (MMBtu/hr)	245
Price of cooling water at 293K per 10 <sup>9</sup> J (\$)	4
Cost of heating fluid at 593K per 10 <sup>9</sup> J (\$)	6



$$\text{Total cash out} = \text{Total raw materials cost} + \text{Total utility cost} + \text{Total fixed cost} - \text{Total income}$$



# Multi-objective Optimization

Cost

Production

Mass  
utilization

Energy  
efficiency

Safety

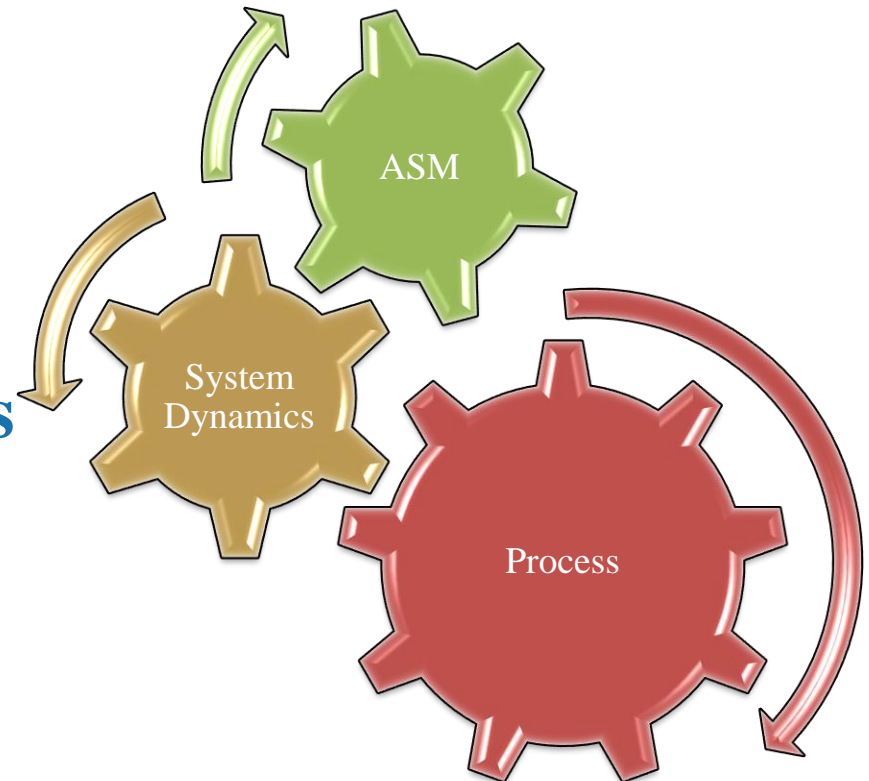
Environmental  
Impact

## Methodology *must*

- Comprehensive
- Systematic
- Generally applicable

## Provide decision makers tools (e.g. Pareto curves)

- Determine optimal flaring strategies/policies



# Outcomes

## So Far.....

- ❑ Historical database of flaring scenarios
  - Ahmed Mhd Nabil AlNouss, Monzure-Khoda Kazi, and Fadwa Eljack. Importance of Process and Flaring Data and its Analysis for the Management of Abnormal Situations - An Ethylene Process Case Study (In preparation).
- ❑ Green house gas calculator
  - Fahd M. Mohammed, Monzure-Khoda Kazi, and Fadwa T. Eljack. Tracking of GHG Emissions and Tax Implication During Normal/Abnormal Situations – Ethylene Process Base Case Industrial Application
- ❑ COGEN – as flare mitigation approach
  - Kamrava, S., Gabriel, K. J., El-Halwagi, M. M., & Eljack, F. T. (2015). Managing abnormal operation through process integration and cogeneration systems. Clean Technologies and Environmental Policy, 1-10.
- ❑ Multi-objective optimization framework
- ❑ Optimal sizing of COGEN
  - Monzure-Khoda Kazi, Fahd Mohammed, Ahmed Mhd Nabil AlNouss and Fadwa Eljack. Multi-objective optimization methodology to size cogeneration systems for managing flares from uncertain sources during abnormal process operation (Submitted in Computers and Chemical Engineering).
- ❑ Potentiality of TMD
  - R.Gonzalez-Bravo, N.A. Elsayed, J.M. Ponce-Ortega, F. Napoles-Rivera, M.M. El-Halwagi, Applied Thermal Engineering (2014)
- ❑ Economic comparison

# Ongoing Works

- Multi-time period method for discrete flare sources
- Impact of fuel quality, energy pricing policy, equipment performance and other external factors related with proposed methodology.
- Optimal design of TMD systems

# Environment vs Economy



# Acknowledgements



## Research Group:

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Engr. Fahd Mohammad

Engr. Ahmed AlNouss



## Collaborators:

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Serveh Kamrava

Kerron Gabriel



Dr. Qiang Xu

Ha Dinh



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**Thank You**

