# Abnormal Situation Management (ASM) in Gas Processing Facilities

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Gas and Fuels Research Initiatives
March 27, 2014
Montgomery, TX











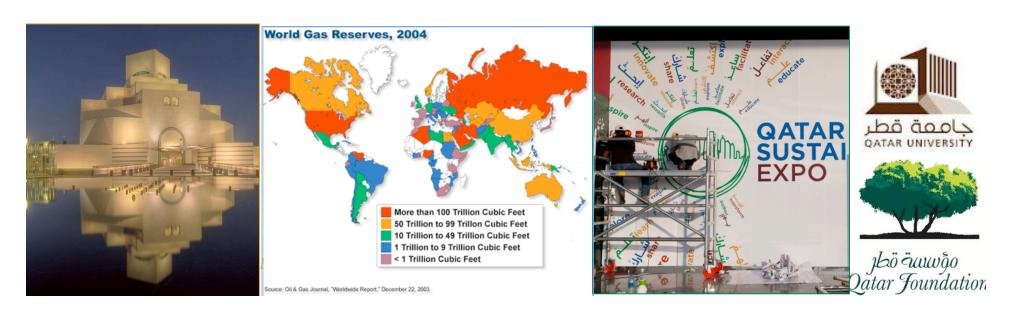








#### Development Oil & Gas Economy Sustainability Education





#### Drop in the Ocean

Despite being almost 90 years old, GTL has seen little commercial application

Name (Location) Company Capacity, barrels per day 140,000 Pearl (Qatar)\* Shell & QP 34,000 Escravos (Nigeria)<sup>2</sup> Chevron & NNPC Oryx (Qatar) Sasol & OP 24,000 Mossel Bay (South Africa) Petro SA 22,500 Bintulu (Malaysia) Shell 14,700

\*Plants under construction Sources: Companies; Deutsche Bank

# PEARL GIL

# DELIVERING THE WORLD'S LARGEST GAS TO LIQUIDS PLANT IN QATAR



#### Qatari Research Investments

Research that support Qatar's vision 2030 and National Priorities

#### **National Priorities**

**Environmental Sustainability** 

Reduce Green House Gas Emissions

Climate Change

#### Infrastructure

QF: Head by First Lady/Sheikha Moza

QNRF: 2.8% National Income ~\$4.8 Billion

Qatar Science and Technology Park, QSTP

QU Research Center/ CEDRA Research Center





**Department of Chemical Engineering** 





A Process-Integration Framework for Abnormal Situation Management (ASM): A Systematic Approach with Application to Qatar's Industrial Needs and Opportunities

#### **Collaborators**















#### Outline

- > Flaring
- > ASM
- > Flare Reduction
- Challenges Motivation
- Approach
- Preliminary Results
- Anticipated Outcomes



## Why Industry Flares?

#### Safety

- Routinely small volumes of unrecoverable gases
- Managing excess gas production

#### **Process Upsets**

- Equipment malfunction
- Off-spec production
- Depressurizing equipment
- Start-ups or Emergency shutdowns







## Why Industry Flares?

#### **Disposal Associated Gases**

- Oil production and gas processing facilities
- Insufficient infrastructure







#### What is Flared?

- Fugitive Emissions7-12% of GHG annual emissions
- Associated GasesMostly methane
- Sweet/Sour Gas
- > Hydrocarbon Vapors
- ➤ Unrecoverable Gases





## Flaring Impact?

30% EU \$10-15 billion losses

23% US NG use

150 Billion m³/yr

400 million T CO2 equivalent

Global gas flaring
has remained
largely stable over
the past fifteen
years, in the range
of 140 to 170
billion cubic meters
(BCM)

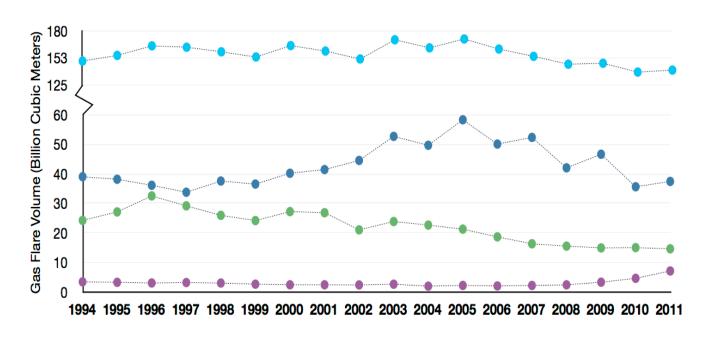
"GE Gas Flaring Report - Recent global trends and policy considerations", 2011.



## Flaring Impact?







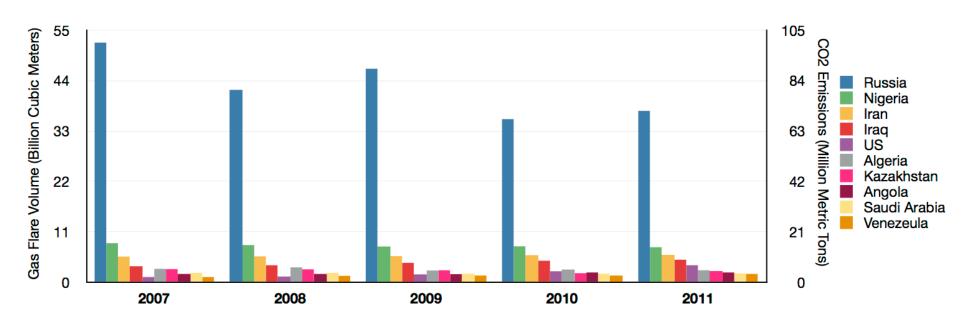
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World

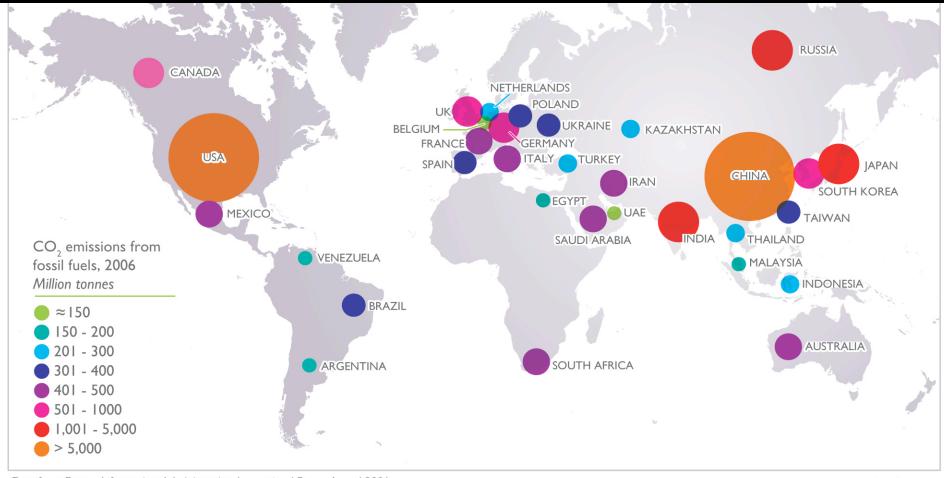
Russia Nigeria US

NOAA (1994-2006); World Bank (2007-2011).





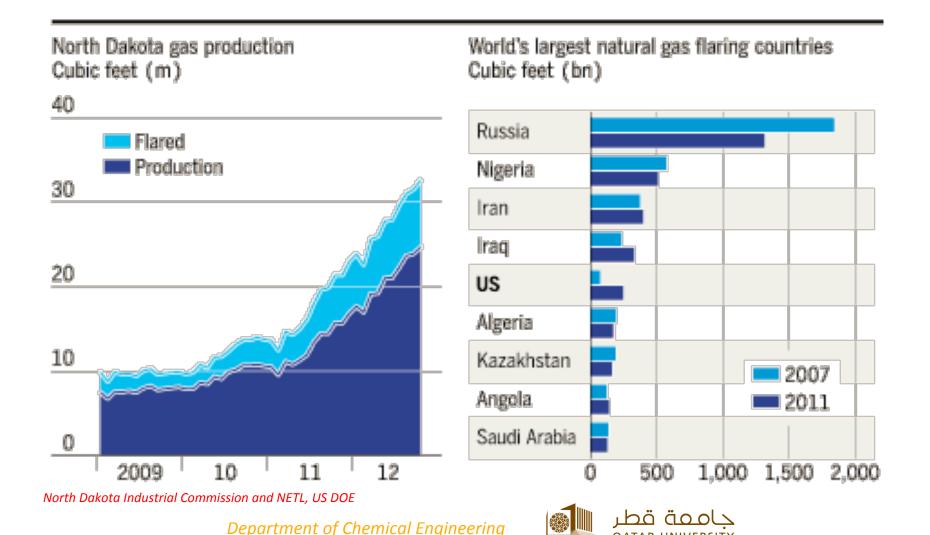


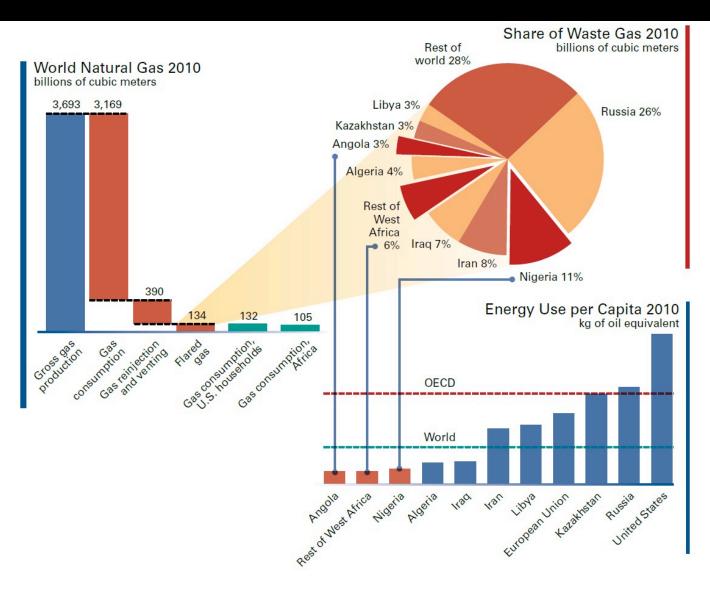


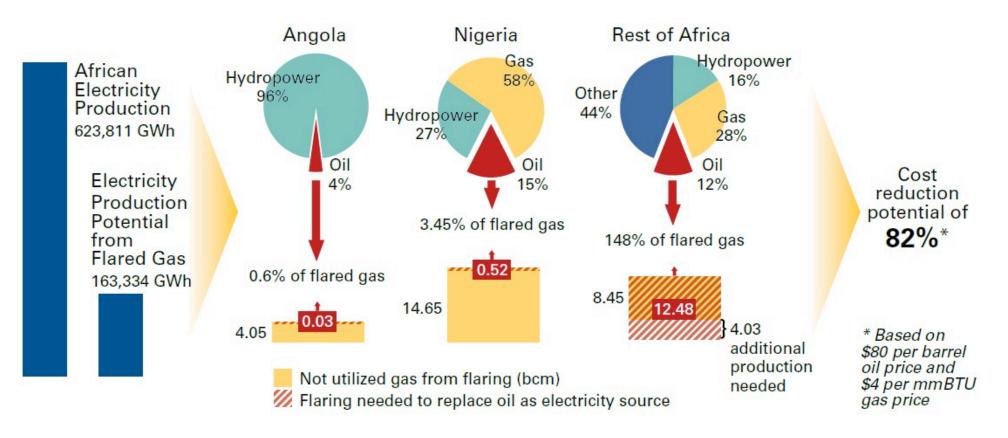
Data from Energy Information Administration International Energy Annual 2006 © CO2CRC

1000 Km Scale at Equator











## Flare Gas Reduction















#### **CHALLENGES**

- > Reducing rates while production levels increase
- Cost effective alternatives
- Cooperation neighboring/competing operators for join facilities

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## Flare Reduction... Why?

Waste valuable resources

Negative Environmental Impacts

<u>Unnecessary CO2/SO2/Nox emissions</u>

**Safety & Economics Impacts** 

Noise - neighboring communities

Visible to surrounding community

Visible black smoke and soot





#### How to Reduce Flaring?

Legislation

Flare recovery

Flare utilization



#### **Qatar's Proactive Legislative Acts**

- '02 Establishing Supreme Council for the Environment
- '05 Kyoto Protocol & '07 AlShaheen CDM Project
- '09 World Bank Global Gas Flaring Reduction (GGFR)
- '12 COP Meeting



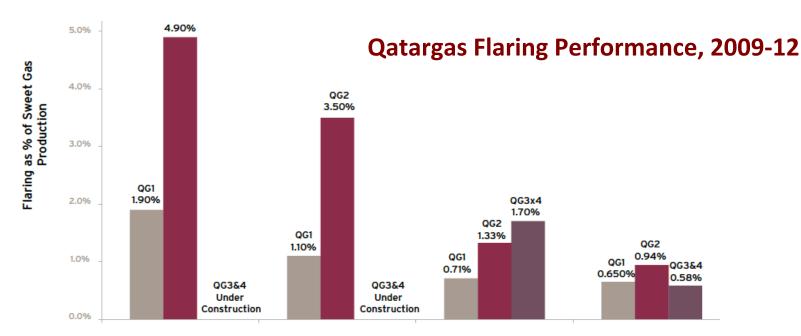
## Qatar Experience

#### Flaring by Subsector

Subsector	Companies Reporting		Flaring (MMSCM)			% Change for Comparable	
	2011	2012	2011	2012	2012 for Comparable Companies	Companies	
LNG/NG	3	3	1,910	2,071	2,071	+8%	
Refining	2	2	2,102	1,202	1,202	-43%	
Oil and gas (E&P)	5	5	596	668	668	+12%	
Petrochemicals	4	5	195	558	385	+98%	



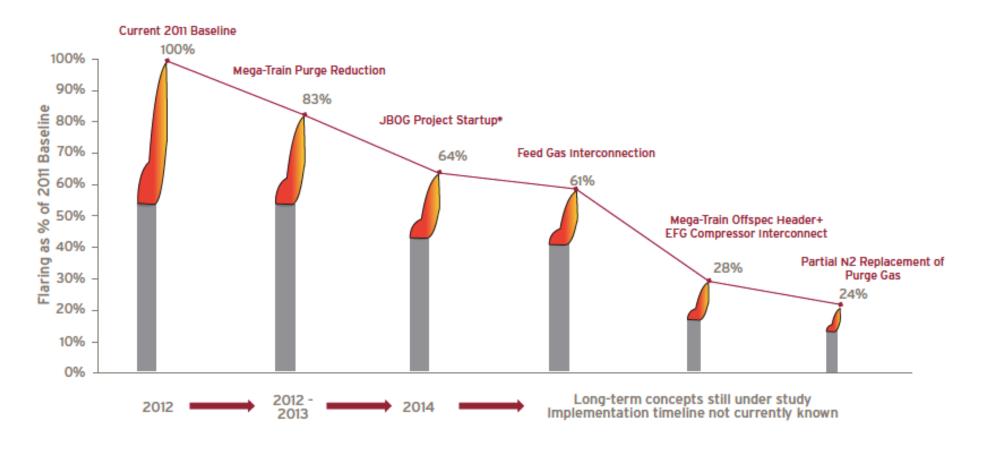
#### How to Reduce Flaring? Qatar Gas



#### 2.9 billion project for flare minimization

- > \$ 1 billion Jetty Boil Off Gas (JBOG) Recovery Project. Sustained baseline flaring rate of around 0.2% of sweet gas (not including unplanned events or planned shutdowns/restarts)
- Recognized November 2012 by World Bank (GGFR)





#### 2.9 billion project for flare minimization

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#### How to Reduce Flaring? QAFAC

#### CO2 Capture Principle Synthesis Gas, H2, C0, C02 Flue Gas from Methanol Conversion the reformer reformer to methanol stack Utilizing Mitsubishi C<sub>02</sub> KS1- solution and process for CO2 capture and release CO2 Capture C<sub>02</sub> Cooling CO2 release Compression process

- > Carbon Dioxide Recovery (CDR) \$300 Million
- ➤ 1st in the world to utilise CO2 captured from flue gas for methanol synthesis



## How to Reduce Flaring? CDM

Legislation

Flare recovery

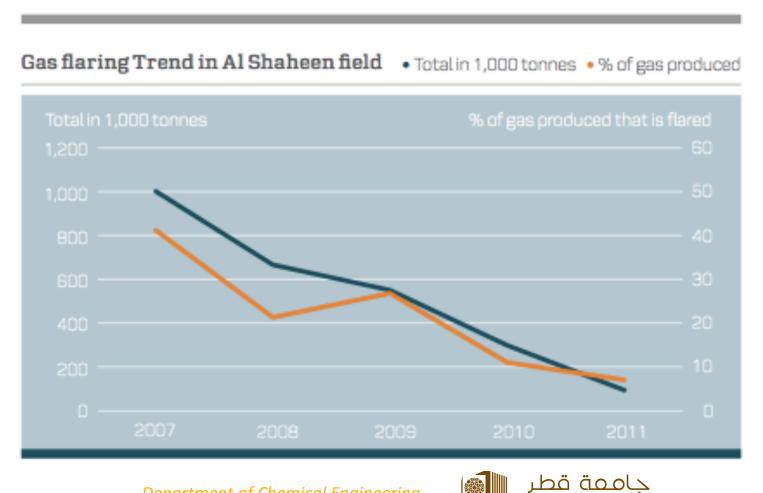
Flare utilization

**Incentives** 

	Country/Year/Name							
	Indonesia 2007 Tambun	Qatar 2007 Al-Shaheen	Nigeria 2008 PanOcean	China 2009 Tarim	Nigeria 2010 Utumu			
Flare Gas Use: Bcm/y	0.1	1.6	1.3	0.2	0.2			
Flare Gas Use: MMcf/d	12.6	150.0	130.0	19.7	16.0			
CO <sub>2</sub> e Total Emissions Reduced: MMT	3.9	17.5	26.3	2.4	2.6			
CO₂e Annual Emissions Reduced: MMT	0.4	2.4	2.6	0.3	0.3			
Capex \$US Million	\$30	\$260	\$302	\$32	\$30			
\$Capex/CO₂e Annually Reduced	\$77	\$106	\$115	\$110	\$117			
\$/MCM Flare Gas Use	\$84	\$60	\$81	\$56	\$65			
\$/MMcfd of Flare Gas Use	\$2.42	\$1.73	\$2.32	\$1.62	\$1.87			
CER Price – \$US/MtCO <sub>2</sub>	\$15	\$6.5	\$7.5	\$10	\$11			
IRR Without Credits (Post Tax)	-30.4%	9.7%	5.4%	11.8%	4.5%			
IRR With Credits (Post Tax)	6.1%	16.0%	11.2%	19.7%	22.4%			
Technology	Mini LPG Plant, Pipeline	Processing, NGL, and Pipeline	Processing, NGL, and Pipeline	Processing, NGL, and Pipeline	Processing, NGL, and Pipeline			



## How to Reduce Flaring? Maersk Oil



#### How to Reduce Flaring?

Legislation

Flare recovery

Flare utilization

**Incentives** 

#### **Associated Gases**

- Reinjection EOR
- Conversion to liquid (easily transported)
- On-site use

**Process** 

- Dynamic Control Systems
- Energy efficiency

Increased demand for productivity/efficiency resulted in sophisticated Control Systems. Yet, they have not eliminated upsets!!

Elvidge, C.D et al. (2009).



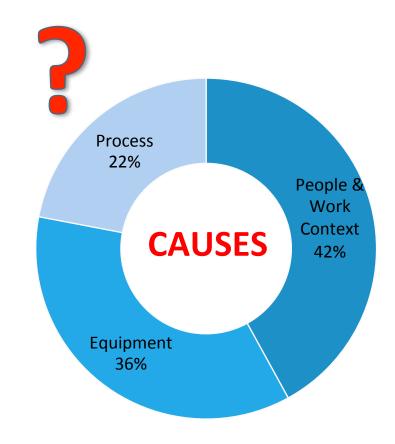


## Process Upsets – Abnormal Situations

Processes eventually deviate from normal operations; and *control system* are in place to *mitigate* such deviations.

When control system *CAN NOT* cope with disturbances , human intervention (DCS operators) is needed

ABNORMAL SITUATIONS



Cochran, E., Bullemer, P. (1996). "ASM: Not by New Technology Alone...", 1996 AlChE conference.

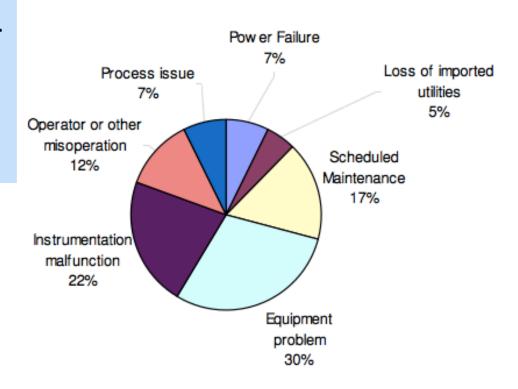


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Midstream Upset Flaring and Management Options, April 2010



## Process Upsets – Abnormal Situations

- Significant in both size and occurrence when compared to routine operation emissions (McCoy et al., 2010)
- Reducing upsets emissions is more effective than reducing routing emissions (Nam et al., 2008)
- Upsets are not random and hence we need to determine if there are means to predict upsets and mitigate accordingly?

Nam, et al. (2008) Journal of Atmospheric Environment 42 B.J. McCoy et al. (2010) Journal of Atmospheric Environment 44





#### Limitation

Currently industry is using a *response* approach to managing abnormal situations

Develop Framework for Optimum

Management of Abnormal Situation

- Proactively preventive & responsive
- Provide both design & operational strategies

roject Objective



# Develop Framework for Optimum Management of Abnormal Situation

Identify key flaring sources due to upsets



Identify causes & consequences of process upsets



Apply recent process design/control and optimization methods

Project Objective



#### Multi-objective Optimization

Cost

Production

Mass utilization

Energy efficiency

Safety

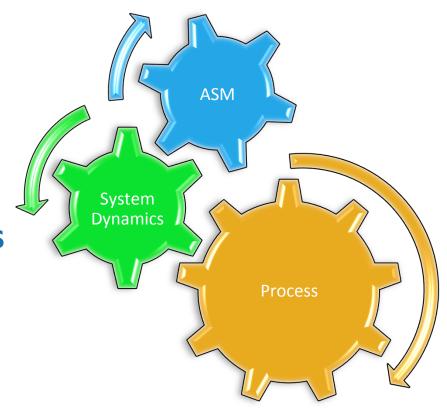
Environmen tal Impact

#### Methodology must

- > Comprehensive
- > Systematic
- Generally applicable

## Provide decision makers tools (e.g. Pareto curves)

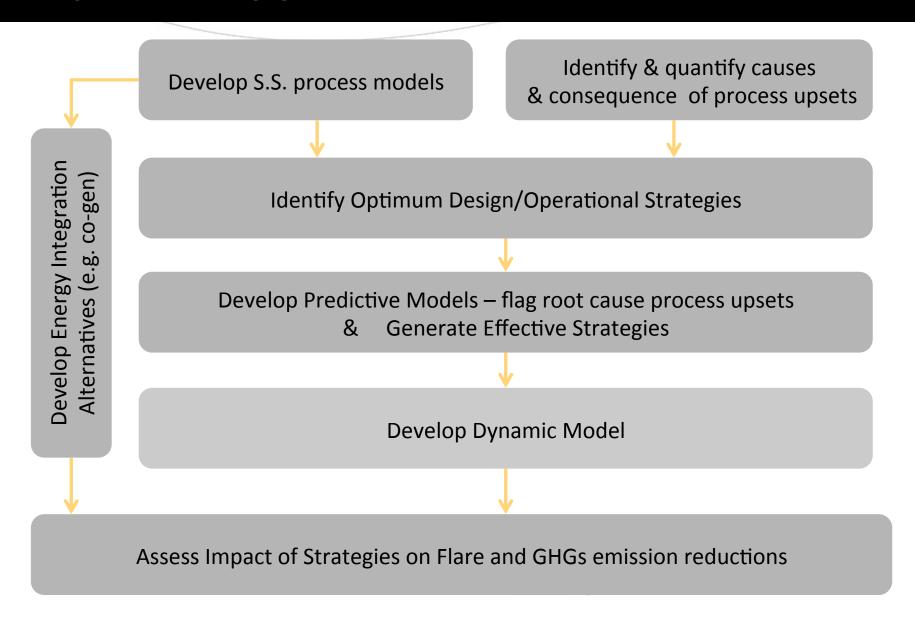
Determine optimal flaring strategies/policies



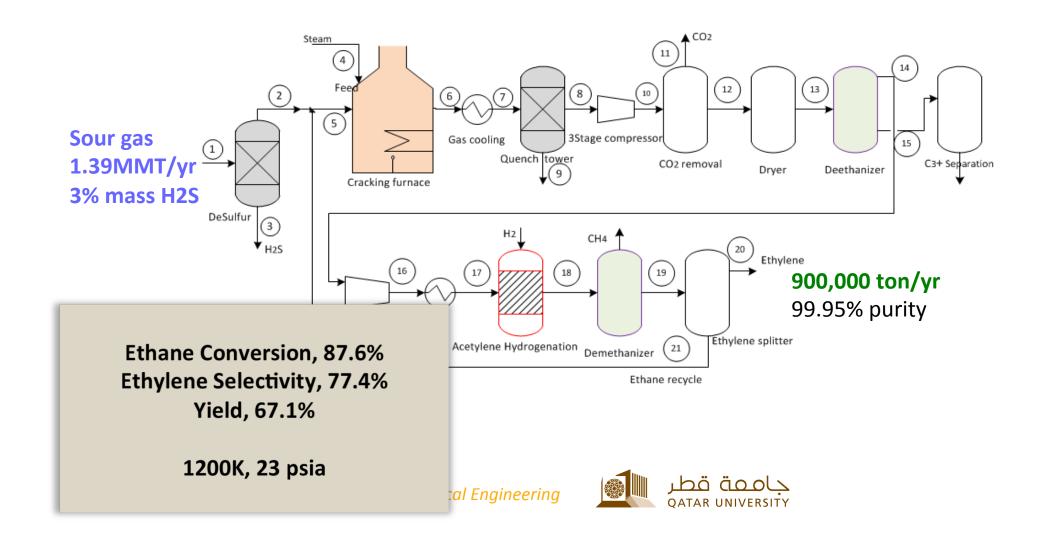


جامعة قطر

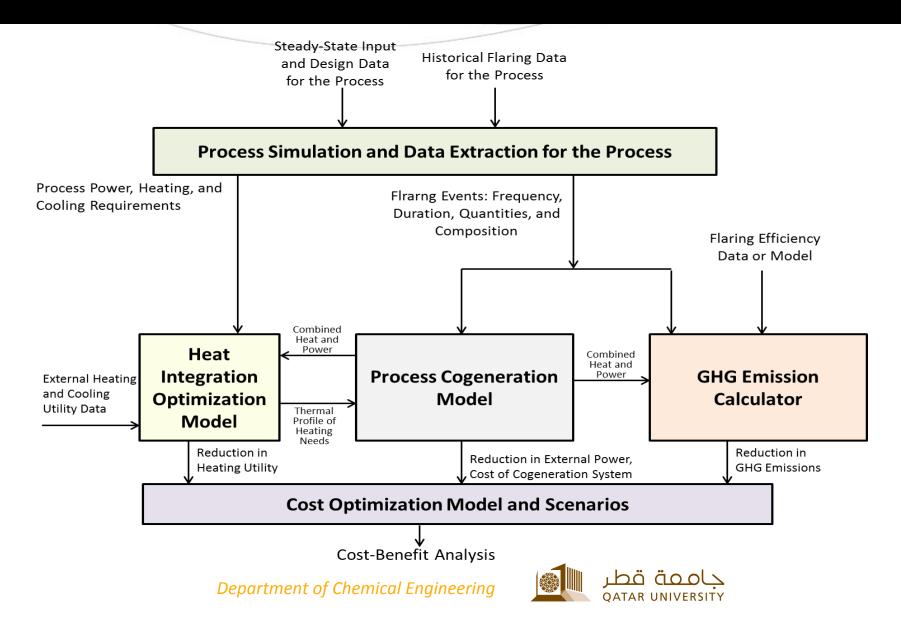
#### **Proposed Approach**



#### **Base Case** Typical Ethylene Process

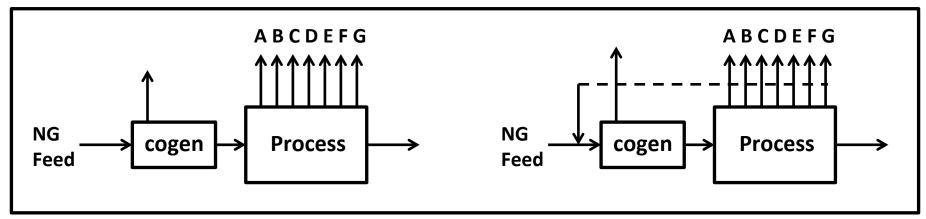


#### Flare Utilization ASM - Cogeneration

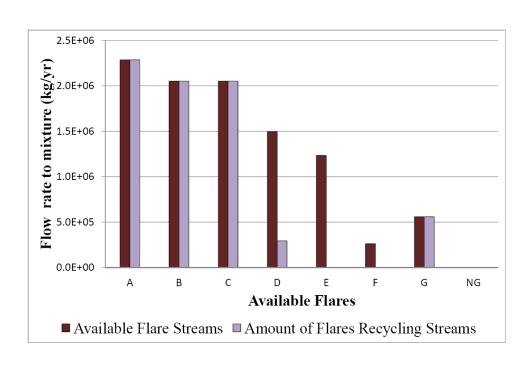


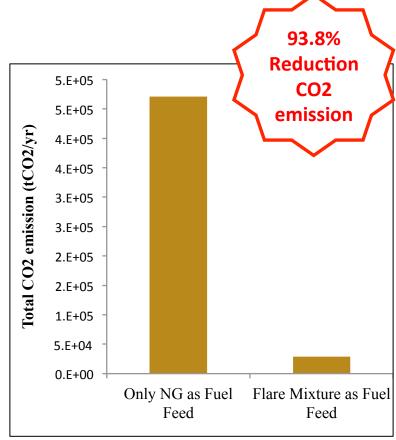
#### Co-gen Design – Assumptions

- > Energy demand is fixed, 40 MMBtu/hr
- Boiler type is fixed
- > All flares are available for feed
- > Given rate of flare streams is an assumed 12 hour/yr per flare
- CO2 emissions estimated using international standards



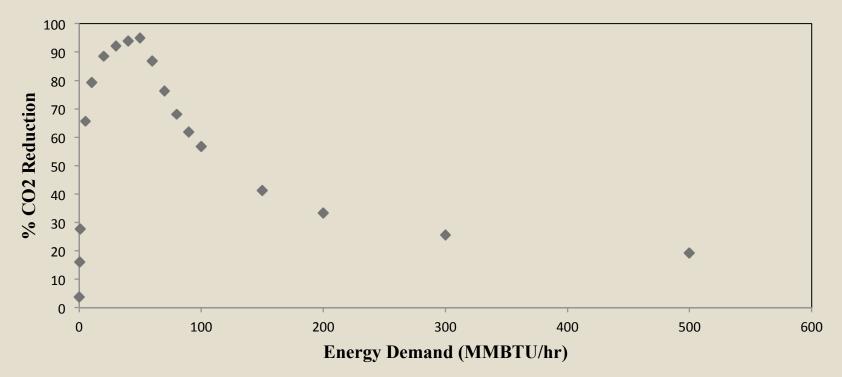
#### Results







#### Energy demand vs. % CO2 reduction after recycling available flare streams



- ➤ Varied energy demand 0.0001 10,000 MMBTU/hr
- > CO2 reductions are realized at all rates
- > Optimality (min CO2 emission) is identified
- True feasibility will be realized upon inclusion of cost into the optimization formulations



#### Project Anticipated Outcomes

- ➤ A working optimization model for data extraction and processing and a database for offering guidance to process engineers and operators
- > A generic approach for modeling causes and effects of process upsets
- A systematic procedures and associated models for the management of abnormal situation.
- ➤ A GHG tracking tool which is linked to different modes of process operation (normal and abnormal)
- An *automated tool* for proposing design and operational changes for process cogeneration (combined heat and power)



# TEXAS A&M







#### **Collaborators**

Prof. Mahmoud El-Halwagi

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Serveh Kamrava

**Fahd Mohammed** 

Kerron Gabriel

Ha Dinh

**Shujing Zhang** 

#### **Funding**

Qatar National Research Fund NPRP 5-351-2-136



Member of Qatar Foundation



National Priorities Research Program







